

Sigurd Skogestad

List of Publications by Year in descending order

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277
papers

12,075
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31976

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282
all docs

282
docs citations

282
times ranked

3849
citing authors

#	ARTICLE	IF	CITATIONS
1	Simple analytic rules for model reduction and PID controller tuning. Journal of Process Control, 2003, 13, 291-309.	3.3	1,535
2	Internal model control: PID controller design. Industrial & Engineering Chemistry Process Design and Development, 1986, 25, 252-265.	0.6	1,247
3	Plantwide control: the search for the self-optimizing control structure. Journal of Process Control, 2000, 10, 487-507.	3.3	505
4	Control structure design for complete chemical plants. Computers and Chemical Engineering, 2004, 28, 219-234.	3.8	349
5	Operation of Integrated Three-Product (Petlyuk) Distillation Columns. Industrial & Engineering Chemistry Research, 1995, 34, 2094-2103.	3.7	238
6	Implications of large RGA-elements on control performance. Industrial & Engineering Chemistry Research, 1987, 26, 2323-2330.	3.7	223
7	Understanding the dynamic behavior of distillation columns. Industrial & Engineering Chemistry Research, 1988, 27, 1848-1862.	3.7	217
8	Estimation of distillation compositions from multiple temperature measurements using partial-least-squares regression. Industrial & Engineering Chemistry Research, 1991, 30, 2543-2555.	3.7	185
9	Simple frequency-dependent tools for control system analysis, structure selection and design. Automatica, 1992, 28, 989-996.	5.0	184
10	Optimal Selection of Controlled Variables. Industrial & Engineering Chemistry Research, 2003, 42, 3273-3284.	3.7	174
11	Robust performance of decentralized control systems by independent designs. Automatica, 1989, 25, 119-125.	5.0	172
12	Plantwide control - A review and a new design procedure. Modeling, Identification and Control, 2000, 21, 209-240.	1.1	171
13	Sequential design of decentralized controllers. Automatica, 1994, 30, 1601-1607.	5.0	151
14	Null Space Method for Selecting Optimal Measurement Combinations as Controlled Variables. Industrial & Engineering Chemistry Research, 2007, 46, 846-853.	3.7	140
15	Optimal measurement combinations as controlled variables. Journal of Process Control, 2009, 19, 138-148.	3.3	134
16	Minimum Energy Consumption in Multicomponent Distillation. 2. Three-Product Petlyuk Arrangements. Industrial & Engineering Chemistry Research, 2003, 42, 605-615.	3.7	123
17	Self-Optimizing Control of a Large-Scale Plant: The Tennessee Eastman Process. Industrial & Engineering Chemistry Research, 2001, 40, 4889-4901.	3.7	120
18	The setpoint overshoot method: A simple and fast closed-loop approach for PID tuning. Journal of Process Control, 2010, 20, 1220-1234.	3.3	119

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19	LV-Control of a high-purity distillation column. Chemical Engineering Science, 1988, 43, 33-48.	3.8	117
20	Effect of disturbance directions on closed-loop performance. Industrial & Engineering Chemistry Research, 1987, 26, 2029-2035.	3.7	112
21	Analysis of instability in an industrial ammonia reactor. AIChE Journal, 1998, 44, 888-895.	3.6	109
22	Selecting the best distillation control configuration. AIChE Journal, 1990, 36, 753-764.	3.6	107
23	Optimal operation of Petlyuk distillation: steady-state behavior. Journal of Process Control, 1999, 9, 407-424.	3.3	105
24	Multiple steady states in ideal two-product distillation. AIChE Journal, 1991, 37, 499-511.	3.6	102
25	Composition estimator in a pilot-plant distillation column using multiple temperatures. Industrial & Engineering Chemistry Research, 1991, 30, 2555-2564.	3.7	101
26	Control configuration selection for distillation columns. AIChE Journal, 1987, 33, 1620-1635.	3.6	99
27	Minimum Energy Consumption in Multicomponent Distillation. 3. More Than Three Products and Generalized Petlyuk Arrangements. Industrial & Engineering Chemistry Research, 2003, 42, 616-629.	3.7	98
28	Minimum Energy Consumption in Multicomponent Distillation. 1. VminDiagram for a Two-Product Column. Industrial & Engineering Chemistry Research, 2003, 42, 596-604.	3.7	98
29	Control structure design for the ammonia synthesis process. Computers and Chemical Engineering, 2008, 32, 2920-2932.	3.8	93
30	Complex distillation arrangements: Extending the petlyuk ideas. Computers and Chemical Engineering, 1997, 21, S237-S242.	3.8	91
31	Self-optimizing control: the missing link between steady-state optimization and control. Computers and Chemical Engineering, 2000, 24, 569-575.	3.8	91
32	Dynamics and Control of Distillation Columns - A Critical Survey. Modeling, Identification and Control, 1997, 18, 177-217.	1.1	90
33	Optimal PI and PID control of first-order plus delay processes and evaluation of the original and improved SIMC rules. Journal of Process Control, 2018, 70, 36-46.	3.3	89
34	Performance weight selection for H-infinity and \hat{H}_∞ -control methods. Transactions of the Institute of Measurement and Control, 1991, 13, 241-252.	1.7	84
35	Economically efficient operation of CO2 capturing process part I: Self-optimizing procedure for selecting the best controlled variables. Chemical Engineering and Processing: Process Intensification, 2011, 50, 247-253.	3.6	83
36	Active Vapor Split Control for Dividing-Wall Columns. Industrial & Engineering Chemistry Research, 2012, 51, 15176-15183.	3.7	81

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37	Tuning for Smooth PID Control with Acceptable Disturbance Rejection. Industrial & Engineering Chemistry Research, 2006, 45, 7817-7822.	3.7	80
38	Energy efficient distillation. Journal of Natural Gas Science and Engineering, 2011, 3, 571-580.	4.4	79
39	An industrial and academic perspective on plantwide control. Annual Reviews in Control, 2011, 35, 99-110.	7.9	75
40	Optimal operation of simple refrigeration cycles. Computers and Chemical Engineering, 2007, 31, 712-721.	3.8	73
41	Economically efficient operation of CO ₂ capturing process. Part II. Design of control layer. Chemical Engineering and Processing: Process Intensification, 2012, 52, 112-124.	3.6	72
42	Dividing wall columns for heterogeneous azeotropic distillation. Chemical Engineering Research and Design, 2015, 99, 111-119.	5.6	70
43	Pairing Criteria for Decentralized Control of Unstable Plants. Industrial & Engineering Chemistry Research, 1994, 33, 2134-2139.	3.7	66
44	Application of plantwide control to the HDA process. "steady-state optimization and self-optimizing control. Control Engineering Practice, 2007, 15, 1222-1237.	5.5	65
45	NCO tracking and self-optimizing control in the context of real-time optimization. Journal of Process Control, 2011, 21, 1407-1416.	3.3	64
46	Design of resilient processing plants-IX. Effect of model uncertainty on dynamic resilience. Chemical Engineering Science, 1987, 42, 1765-1780.	3.8	62
47	SVD controllers for H ₂ , H _∞ and 1/4-optimal control. Automatica, 1997, 33, 433-439.	5.0	62
48	Coordinator MPC for maximizing plant throughput. Computers and Chemical Engineering, 2008, 32, 195-204.	3.8	62
49	Control of fuel cell power output. Journal of Process Control, 2007, 17, 333-347.	3.3	60
50	Multivessel batch distillation. AIChE Journal, 1997, 43, 971-978.	3.6	56
51	Controllability analysis of two-phase pipeline-riser systems at riser slugging conditions. Control Engineering Practice, 2007, 15, 567-581.	5.5	56
52	Steady-state real-time optimization using transient measurements. Computers and Chemical Engineering, 2018, 115, 34-45.	3.8	56
53	Dynamic behaviour of integrated plants. Journal of Process Control, 1996, 6, 145-156.	3.3	54
54	Output estimation using multiple secondary measurements: High-purity distillation. AIChE Journal, 1993, 39, 1641-1653.	3.6	52

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55	Shortcut Analysis of Optimal Operation of Petlyuk Distillation. Industrial & Engineering Chemistry Research, 2004, 43, 3994-3999.	3.7	52
56	Comparison of regular and inverted batch distillation. Chemical Engineering Science, 1996, 51, 4949-4962.	3.8	51
57	A Natural Gas to Liquids Process Model for Optimal Operation. Industrial & Engineering Chemistry Research, 2012, 51, 425-433.	3.7	50
58	Integrating operations and control: A perspective and roadmap for future research. Computers and Chemical Engineering, 2018, 115, 179-184.	3.8	50
59	Representation of uncertain time delays in the Håžframework. International Journal of Control, 1994, 59, 627-638.	1.9	49
60	Improved independent design of robust decentralized controllers. Journal of Process Control, 1993, 3, 43-51.	3.3	48
61	Hydraulic design, technical challenges and comparison of alternative configurations of a four-product dividing wall column. Chemical Engineering and Processing: Process Intensification, 2014, 84, 71-81.	3.6	48
62	Effects of recycle on dynamics and control of chemical processing plants. Computers and Chemical Engineering, 1994, 18, S529-S534.	3.8	47
63	Optimal operation of Kaibel distillation columns. Chemical Engineering Research and Design, 2011, 89, 1382-1391.	5.6	46
64	Real-Time Optimization under Uncertainty Applied to a Gas Lifted Well Network. Processes, 2016, 4, 52.	2.8	46
65	Optimizing control of Petlyuk distillation: Understanding the steady-state behavior. Computers and Chemical Engineering, 1997, 21, S249-S254.	3.8	44
66	Multi-effect distillation applied to an industrial case study. Chemical Engineering and Processing: Process Intensification, 2005, 44, 819-826.	3.6	44
67	Total reflux operation of multivessel batch distillation. Computers and Chemical Engineering, 1996, 20, S1041-S1046.	3.8	43
68	Optimal operation of simple refrigeration cycles. Computers and Chemical Engineering, 2007, 31, 1590-1601.	3.8	43
69	Inadequacy of steady-state analysis for feedback control: distillate-bottom control of distillation columns. Industrial & Engineering Chemistry Research, 1990, 29, 2339-2346.	3.7	42
70	Inconsistencies in Dynamic Models for Ill-Conditioned Plants: Application to Low-Order Models of Distillation Columns. Industrial & Engineering Chemistry Research, 1994, 33, 631-640.	3.7	41
71	Near-optimal operation by self-optimizing control: from process control to marathon running and business systems. Computers and Chemical Engineering, 2004, 29, 127-137.	3.8	41
72	Control structure selection for three-product Petlyuk (dividing-wall) column. Chemical Engineering and Processing: Process Intensification, 2013, 64, 57-67.	3.6	41

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73	Comparison of Various Control Configurations for Continuous Bioreactors. <i>Industrial & Engineering Chemistry Research</i> , 1997, 36, 697-705.	3.7	39
74	Buffer Tank Design for Acceptable Control Performance. <i>Industrial & Engineering Chemistry Research</i> , 2003, 42, 2198-2208.	3.7	39
75	Control structure design for optimal operation of heat exchanger networks. <i>AIChE Journal</i> , 2008, 54, 150-162.	3.6	39
76	Selection of Controlled Variables and Robust Setpoints. <i>Industrial & Engineering Chemistry Research</i> , 2005, 44, 2207-2217.	3.7	38
77	Application of Plantwide Control to the HDA Process. IIRegulatory Control. <i>Industrial & Engineering Chemistry Research</i> , 2007, 46, 5159-5174.	3.7	38
78	Convex formulations for optimal selection of controlled variables and measurements using Mixed Integer Quadratic Programming. <i>Journal of Process Control</i> , 2012, 22, 995-1007.	3.3	38
79	Data reconciliation and optimal operation of a catalytic naphtha reformer. <i>Journal of Process Control</i> , 2008, 18, 320-331.	3.3	37
80	Model predictive control for the self-optimized operation in wastewater treatment plants: Analysis of dynamic issues. <i>Computers and Chemical Engineering</i> , 2015, 82, 259-272.	3.8	36
81	Consistent Inventory Control. <i>Industrial & Engineering Chemistry Research</i> , 2009, 48, 10892-10902.	3.7	35
82	Steady State and Dynamic Operation of Four-Product Dividing-Wall (Kaibel) Columns: Experimental Verification. <i>Industrial & Engineering Chemistry Research</i> , 2012, 51, 15696-15709.	3.7	35
83	Control structure selection for four-product Kaibel column. <i>Computers and Chemical Engineering</i> , 2016, 93, 372-381.	3.8	34
84	Dynamic models for heat exchangers and heat exchanger networks. <i>Computers and Chemical Engineering</i> , 1994, 18, S459-S463.	3.8	33
85	Control-oriented modelling and experimental study of the transient response of a high-temperature polymer fuel cell. <i>Journal of Power Sources</i> , 2006, 162, 215-227.	7.8	33
86	Control structure selection for four-product Petlyuk column. <i>Chemical Engineering and Processing: Process Intensification</i> , 2013, 67, 49-59.	3.6	33
87	Model Predictive Control of Reactive Dividing Wall Column for the Selective Hydrogenation and Separation of a C3 Stream in an Ethylene Plant. <i>Industrial & Engineering Chemistry Research</i> , 2016, 55, 9738-9748.	3.7	33
88	Single-cycle mixed-fluid LNG process Part I: Optimal design. , 2009, , 211-218.		31
89	Chemical and Energy Process Engineering. , 0, , .		30
90	Problems with Specifying T_{min} in the Design of Processes with Heat Exchangers. <i>Industrial & Engineering Chemistry Research</i> , 2008, 47, 3071-3075.	3.7	28

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91	Self-optimizing control with active set changes. <i>Journal of Process Control</i> , 2012, 22, 873-883.	3.3	28
92	Control structure design and dynamic modeling for a solid oxide fuel cell with direct internal reforming of methane. <i>Chemical Engineering Research and Design</i> , 2015, 98, 202-211.	5.6	28
93	Bypass selection for control of heat exchanger networks. <i>Computers and Chemical Engineering</i> , 1992, 16, S263-S272.	3.8	27
94	Control strategies for reactive batch distillation. <i>Journal of Process Control</i> , 1994, 4, 205-217.	3.3	27
95	Temperature Cascade Control of Distillation Columns. <i>Industrial & Engineering Chemistry Research</i> , 1996, 35, 475-484.	3.7	27
96	Selection of Controlled Variables: Maximum Gain Rule and Combination of Measurements. <i>Industrial & Engineering Chemistry Research</i> , 2008, 47, 9465-9471.	3.7	27
97	Optimal operation of heat exchanger networks with stream split: Only temperature measurements are required. <i>Computers and Chemical Engineering</i> , 2014, 70, 35-49.	3.8	27
98	Relative Gain Array for Norm-Bounded Uncertain Systems. <i>Industrial & Engineering Chemistry Research</i> , 2006, 45, 1751-1757.	3.7	26
99	Dynamic considerations in the synthesis of self-optimizing control structures. <i>AIChE Journal</i> , 2008, 54, 1830-1841.	3.6	26
100	Control of the mass and energy dynamics of polybenzimidazole-membrane fuel cells. <i>Journal of Process Control</i> , 2009, 19, 415-432.	3.3	26
101	Steady-State Operational Degrees of Freedom with Application to Refrigeration Cycles. <i>Industrial & Engineering Chemistry Research</i> , 2009, 48, 6652-6659.	3.7	26
102	Instability of distillation columns. <i>AIChE Journal</i> , 1994, 40, 1466-1478.	3.6	25
103	pH-neutralization: integrated process and control design. <i>Computers and Chemical Engineering</i> , 2004, 28, 1475-1487.	3.8	23
104	Minimum energy diagrams for multieffect distillation arrangements. <i>AIChE Journal</i> , 2005, 51, 1714-1725.	3.6	22
105	Plantwide Control for Economic Optimum Operation of a Recycle Process with Side Reaction. <i>Industrial & Engineering Chemistry Research</i> , 2011, 50, 8571-8584.	3.7	22
106	Real-Time optimization as a feedback control problem – A review. <i>Computers and Chemical Engineering</i> , 2022, 161, 107723.	3.8	22
107	Multiple Steady States and Instability in Distillation. Implications for Operation and Control. <i>Industrial & Engineering Chemistry Research</i> , 1995, 34, 4395-4405.	3.7	21
108	Perfect Steady-State Indirect Control. <i>Industrial & Engineering Chemistry Research</i> , 2005, 44, 863-867.	3.7	21

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109	Optimal controlled variables for polynomial systems. <i>Journal of Process Control</i> , 2012, 22, 167-179.	3.3	21
110	Economic Plantwide Control of the Cumene Process. <i>Industrial & Engineering Chemistry Research</i> , 2013, 52, 830-846.	3.7	21
111	Active constraint regions for a natural gas liquefaction process. <i>Journal of Natural Gas Science and Engineering</i> , 2013, 10, 8-13.	4.4	21
112	Sensitivity Analysis of Optimal Operation of an Activated Sludge Process Model for Economic Controlled Variable Selection. <i>Industrial & Engineering Chemistry Research</i> , 2013, 52, 9908-9921.	3.7	21
113	Optimal operation and stabilising control of the concentric heat-integrated distillation column (HiDiC). <i>Computers and Chemical Engineering</i> , 2017, 96, 196-211.	3.8	21
114	On combining self-optimizing control and extremum-seeking control – Applied to an ammonia reactor case study. <i>Journal of Process Control</i> , 2019, 78, 78-87.	3.3	21
115	Small-scale experiments on stabilizing riser slug flow. <i>Chemical Engineering Research and Design</i> , 2010, 88, 213-228.	5.6	20
116	Robust control of time-delay systems using the Smith predictor. <i>International Journal of Control</i> , 1993, 57, 1405-1420.	1.9	19
117	Feedback Real-Time Optimization Strategy Using a Novel Steady-state Gradient Estimate and Transient Measurements. <i>Industrial & Engineering Chemistry Research</i> , 2019, 58, 207-216.	3.7	19
118	Robust control of homogeneous azeotropic distillation columns. <i>AIChE Journal</i> , 1991, 37, 1810-1824.	3.6	18
119	Effect of RHP zeros and poles on the sensitivity functions in multivariable systems. <i>Journal of Process Control</i> , 1998, 8, 155-164.	3.3	18
120	Offset-Free Tracking of Model Predictive Control with Model Mismatch: Experimental Results. <i>Industrial & Engineering Chemistry Research</i> , 2005, 44, 3966-3972.	3.7	18
121	A Sensory-Motor Control Model of Animal Flight Explains Why Bats Fly Differently in Light Versus Dark. <i>PLoS Biology</i> , 2015, 13, e1002046.	5.6	18
122	Opportunities and difficulties with 5 Å– 5 distillation control. <i>Journal of Process Control</i> , 1995, 5, 249-261.	3.3	17
123	Computational performance of aggregated distillation models. <i>Computers and Chemical Engineering</i> , 2009, 33, 296-308.	3.8	17
124	Active Constraint Regions for Optimal Operation of Chemical Processes. <i>Industrial & Engineering Chemistry Research</i> , 2011, 50, 11226-11236.	3.7	17
125	Economic Plantwide Control Over a Wide Throughput Range: A Systematic Design Procedure. <i>AIChE Journal</i> , 2013, 59, 2407-2426.	3.6	17
126	Simultaneous design of proportional–integral–derivative controller and measurement filter by optimisation. <i>IET Control Theory and Applications</i> , 2017, 11, 341-348.	2.1	17

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127	Consistency of steady-state models using insight about extensive variables. <i>Industrial & Engineering Chemistry Research</i> , 1991, 30, 654-661.	3.7	16
128	Feedforward Control under the Presence of Uncertainty*. <i>European Journal of Control</i> , 2004, 10, 30-46.	2.6	16
129	Simple Rules for Economic Plantwide Control. <i>Computer Aided Chemical Engineering</i> , 2015, 37, 101-108.	0.5	16
130	Systematic Design of Active Constraint Switching Using Classical Advanced Control Structures. <i>Industrial & Engineering Chemistry Research</i> , 2020, 59, 2229-2241.	3.7	16
131	Multi-input single-output control for extending the operating range: Generalized split range control using the baton strategy. <i>Journal of Process Control</i> , 2020, 91, 1-11.	3.3	16
132	Evaluation of Dynamic Models of Distillation Columns with Emphasis on the Initial Response. <i>Modeling, Identification and Control</i> , 2000, 21, 83-103.	1.1	16
133	Reactor/separator processes with recycles-2. Design for composition control. <i>Computers and Chemical Engineering</i> , 2003, 27, 401-421.	3.8	15
134	Control structure comparison for three-product Petlyuk column. <i>Chinese Journal of Chemical Engineering</i> , 2018, 26, 1621-1630.	3.5	15
135	Optimal operation of oil and gas production using simple feedback control structures. <i>Control Engineering Practice</i> , 2019, 91, 104107.	5.5	15
136	Comparison of stabilizing control structures for dividing wall columns. <i>IFAC-PapersOnLine</i> , 2016, 49, 729-734.	0.9	14
137	A simple dynamic gravity separator model for separation efficiency evaluation incorporating level and pressure control. , 2017, , .		14
138	Improving Scenario Decomposition for Multistage MPC Using a Sensitivity-Based Path-Following Algorithm. , 2018, 2, 581-586.		14
139	Online Process Optimization with Active Constraint Set Changes using Simple Control Structures. <i>Industrial & Engineering Chemistry Research</i> , 2019, 58, 13555-13567.	3.7	14
140	Control of Unstable Distillation Columns. , 1991, , .		13
141	Closed operation of multivessel batch distillation: Experimental verification. <i>AIChE Journal</i> , 2000, 46, 1209-1217.	3.6	13
142	Plantwide control: Towards a systematic procedure. <i>Computer Aided Chemical Engineering</i> , 2002, 10, 57-69.	0.5	13
143	Identification and analysis of possible splits for azeotropic mixturesâ€™1. Method for column sections. <i>Chemical Engineering Science</i> , 2011, 66, 2512-2522.	3.8	13
144	Anti-slug control solutions based on identified model. <i>Journal of Process Control</i> , 2015, 30, 58-68.	3.3	13

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145	Dividing-Wall Column for Fractionation of Natural Gas Liquids in Floating Liquefied Natural Gas Plants. <i>Chemical Engineering and Technology</i> , 2016, 39, 2348-2354.	1.5	13
146	Anti-slug control based on a virtual flow measurement. <i>Flow Measurement and Instrumentation</i> , 2017, 53, 299-307.	2.0	13
147	A Distributed Algorithm for Scenario-based Model Predictive Control using Primal Decomposition. <i>IFAC-PapersOnLine</i> , 2018, 51, 351-356.	0.9	13
148	Optimal Operation with Changing Active Constraint Regions using Classical Advanced Control. <i>IFAC-PapersOnLine</i> , 2018, 51, 440-445.	0.9	13
149	Scaled steady state models for effective on-line applications. <i>Computers and Chemical Engineering</i> , 2008, 32, 990-999.	3.8	12
150	Medium-Scale Experiments on Stabilizing Riser-Slug Flow. <i>SPE Projects, Facilities and Construction</i> , 2009, 4, 156-170.	0.2	12
151	Controllability analysis of severe slugging in well-pipeline-riser systems. <i>IFAC Postprint Volumes IPPV / International Federation of Automatic Control</i> , 2012, 45, 101-108.	0.4	12
152	A First-Principles Approach for Control-Oriented Modeling of De-oiling Hydrocyclones. <i>Industrial & Engineering Chemistry Research</i> , 2020, 59, 18937-18950.	3.7	12
153	Experience in Norsk Hydro with cubic equations of state. <i>Fluid Phase Equilibria</i> , 1983, 13, 179-188.	2.5	11
154	Selection of Controlled Variables for a Natural Gas to Liquids Process. <i>Industrial & Engineering Chemistry Research</i> , 2012, 51, 10179-10190.	3.7	11
155	Gas Lift Optimization under Uncertainty. <i>Computer Aided Chemical Engineering</i> , 2017, 40, 1753-1758.	0.5	11
156	Dynamic self-optimizing control for unconstrained batch processes. <i>Computers and Chemical Engineering</i> , 2018, 117, 451-468.	3.8	11
157	A Primal decomposition algorithm for distributed multistage scenario model predictive control. <i>Journal of Process Control</i> , 2019, 81, 162-171.	3.3	11
158	Systematic design of active constraint switching using selectors. <i>Computers and Chemical Engineering</i> , 2020, 143, 107106.	3.8	11
159	Optimal Resource Allocation using Distributed Feedback-based Real-time Optimization. <i>IFAC-PapersOnLine</i> , 2021, 54, 706-711.	0.9	11
160	Controller design for serial processes. <i>Journal of Process Control</i> , 2005, 15, 259-271.	3.3	10
161	Reduced distillation models via stage aggregation. <i>Chemical Engineering Science</i> , 2010, 65, 3439-3456.	3.8	10
162	Manipulation of vapour split in Kaibel distillation arrangements. <i>Chemical Engineering and Processing: Process Intensification</i> , 2013, 72, 10-23.	3.6	10

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163	Improved PI control for a surge tank satisfying level constraints – This work was supported in part by the Norwegian Research Council under the project SUBPRO (Subsea production and processing).. IFAC-PapersOnLine, 2018, 51, 835-840.	0.9	10
164	Optimization of fixed-order controllers using exact gradients. Journal of Process Control, 2018, 71, 130-138.	3.3	10
165	Multiple-Input Single-Output Control for Extending the Steady-State Operating Range – Use of Controllers with Different Setpoints. Processes, 2019, 7, 941.	2.8	10
166	Optimal operation and control of heat to power cycles: A new perspective from a systematic plantwide control approach. Computers and Chemical Engineering, 2020, 141, 106995.	3.8	10
167	Linear parameter-varying model for a refuellable zinc – air battery. Royal Society Open Science, 2020, 7, 201107.	2.4	10
168	A systematic approach to the design of buffer tanks. Computers and Chemical Engineering, 2000, 24, 1395-1401.	3.8	9
169	Approach for efficient computation of disturbance rejection measures for feedback control. Journal of Process Control, 2007, 17, 501-508.	3.3	9
170	Global Self-Optimizing Control for Uncertain Constrained Process Systems * *The author L. Ye gratefully acknowledge the National Natural Science Foundation of China (NSFC) (61673349, 61304081), Ningbo Natural Science Foundation (2015A610151) and China Scholarship Council (No. 201508330751). IFAC-PapersOnLine, 2017, 50, 4672-4677.	0.9	9
171	Systematic Design of Split Range Controllers. IFAC-PapersOnLine, 2019, 52, 898-903.	0.9	9
172	Branch and bound methods for control structure design. Computer Aided Chemical Engineering, 2006, 21, 1371-1376.	0.5	8
173	Identification and analysis of possible splits for azeotropic mixtures. 2. Method for simple columns. Chemical Engineering Science, 2012, 69, 159-169.	3.8	8
174	Profitable and dynamically feasible operating point selection for constrained processes. Journal of Process Control, 2014, 24, 531-541.	3.3	8
175	Optimal operation of energy storage in buildings: Use of the hot water system. Journal of Energy Storage, 2016, 5, 102-112.	8.1	8
176	Control structure design of a solid oxide fuel cell and a molten carbonate fuel cell integrated system: Top-down analysis. Energy Conversion and Management, 2017, 152, 88-98.	9.2	8
177	Control-oriented modelling of gas-liquid cylindrical cyclones. , 2017, , .		8
178	A Control- and Estimation-Oriented Gravity Separator Model for Oil and Gas Applications Based upon First-Principles. Industrial & Engineering Chemistry Research, 2018, 57, 7201-7217.	3.7	8
179	Self-Optimizing Control in Chemical Recycle Processes. IFAC-PapersOnLine, 2018, 51, 536-541.	0.9	8
180	Surrogate model generation using self-optimizing variables. Computers and Chemical Engineering, 2018, 119, 143-151.	3.8	8

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181	The use of first principles model for evaluation of adaptive soft sensor for multicomponent distillation unit. <i>Chemical Engineering Research and Design</i> , 2019, 151, 70-78.	5.6	8
182	A new termination criterion for sampling for surrogate model generation using partial least squares regression. <i>Computers and Chemical Engineering</i> , 2019, 121, 75-85.	3.8	8
183	Modelling and Identification for Robust Control of Ill-Conditioned Plants - a Distillation Case Study. , 1991, , .		8
184	Loopshaping for robust performance. <i>International Journal of Robust and Nonlinear Control</i> , 1996, 6, 805-823.	3.7	7
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