Jorge Ancheyta

List of Publications by Year in descending order

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Version: 2024-02-01

71102 85541 6,116 135 41 71 citations h-index g-index papers 141 141 141 2771 docs citations times ranked citing authors all docs

#	Article	IF	CITATIONS
1	Kinetic modeling of aquathermolysis for upgrading of heavy oils. Fuel, 2022, 310, 122286.	6.4	30
2	Selection of heavy oil upgrading technologies by proper estimation of petroleum prices. Petroleum Science and Technology, 2022, 40, 217-236.	1.5	4
3	Modeling and simulation of a multi-bed industrial reactor for renewable diesel hydroprocessing. Renewable Energy, 2022, 186, 173-182.	8.9	4
4	Modeling of the Deasphalting Process by a Residue–Solvent Equilibrium Calculation Using Continuous Thermodynamics. Industrial & Engineering Chemistry Research, 2022, 61, 3383-3394.	3.7	1
5	Catalyst Stacking Technology as a Viable Solution to Ultralow Sulfur Diesel Production. Energy & Energ	5.1	8
6	Kinetics of heavy oil non-catalytic aquathermolysis with and without stoichiometric coefficients. Fuel, 2022, 323, 124365.	6.4	10
7	Analysis of kinetic models for hydrocracking of heavy oils for In-situ and Ex-situ applications. Fuel, 2022, 323, 124322.	6.4	10
8	SARA-based kinetic model for non-catalytic aquathermolysis of heavy crude oil. Journal of Petroleum Science and Engineering, 2022, 216, 110845.	4.2	21
9	Evaluation of mixing rules to predict viscosity of petrodiesel and biodiesel blends. Fuel, 2021, 283, 118941.	6.4	15
10	Evaluation and comparison of thermodynamic and kinetic parameters for oxidation and pyrolysis of Yarega heavy crude oil asphaltenes. Fuel, 2021, 297, 120703.	6.4	12
11	Prediction of Temperature Profiles for Catalytic Hydrotreating of Vegetable Oil with a Robust Dynamic Reactor Model. Industrial & Engineering Chemistry Research, 2021, 60, 13812-13821.	3.7	4
12	Evaluation of Asphaltene Stability of a Wide Range of Mexican Crude Oils. Energy & Evaluation of Asphaltene Stability of a Wide Range of Mexican Crude Oils. Energy & Evaluation of Asphaltene Stability of a Wide Range of Mexican Crude Oils. Energy & Evaluation of Asphaltene Stability of a Wide Range of Mexican Crude Oils. Energy & Evaluation of Asphaltene Stability of a Wide Range of Mexican Crude Oils. Energy & Evaluation of Asphaltene Stability of a Wide Range of Mexican Crude Oils. Energy & Evaluation of Asphaltene Stability of a Wide Range of Mexican Crude Oils. Energy & Evaluation of Asphaltene Stability of a Wide Range of Mexican Crude Oils. Energy & Evaluation of Asphaltene Stability of Evaluation of Asphaltene Stability of Evaluation of Eval	5.1	15
13	Regular solution model to predict the asphaltenes flocculation and sediments formation during hydrocracking of heavy oil. Fuel, 2020, 260, 116160.	6.4	11
14	Catalytic hydrocracking of a Mexican heavy oil on a MoS2/Al2O3 catalyst: I. Study of the transformation of isolated saturates fraction obtained from SARA analysis. Catalysis Today, 2020, 353, 153-162.	4.4	6
15	Modeling of a bench-scale fixed-bed reactor for catalytic hydrotreating of vegetable oil. Renewable Energy, 2020, 148, 790-797.	8.9	10
16	State estimation for heavy oil hydroprocessing reactors using extended Kalman filters. Fuel, 2020, 262, 116565.	6.4	5
17	Thermogravimetric Determination of the Kinetics of Petroleum Needle Coke Formation by Decantoil Thermolysis. ACS Omega, 2020, 5, 29570-29576.	3.5	6
18	Scaling Up the Performance of a Reactor Model for Hydrotreating Vegetable Oil from Bench-Scale to Pilot-Scale Reactors. Industrial & Engineering Chemistry Research, 2020, 59, 21712-21719.	3.7	5

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19	Batch Reactor Study for Partial Upgrading of a Heavy Oil with a Novel Solid Hydrogen Transfer Agent. Energy & E	5.1	3
20	Kinetic models for Fischer-Tropsch synthesis for the production of clean fuels. Catalysis Today, 2020, 353, 3-16.	4.4	32
21	Modeling and control of a Fischer-Tropsch synthesis fixed-bed reactor with a novel mechanistic kinetic approach. Chemical Engineering Journal, 2020, 390, 124489.	12.7	13
22	Hydrodeoxygenation of vegetable oil in batch reactor: Experimental considerations. Chinese Journal of Chemical Engineering, 2020, 28, 1670-1683.	3.5	10
23	Revisiting the importance of appropriate parameter estimation based on sensitivity analysis for developing kinetic models. Fuel, 2020, 267, 117113.	6.4	15
24	Simulation of bench-scale hydrotreating of vegetable oil reactor under non-isothermal conditions. Fuel, 2020, 275, 117960.	6.4	3
25	Importance of proper hydrodynamics modelling in fixedâ€bed reactors: Fischerâ€Tropsch synthesis study case. Canadian Journal of Chemical Engineering, 2019, 97, 2685-2698.	1.7	2
26	Using Separate Kinetic Models to Predict Liquid, Gas, and Coke Yields in Heavy Oil Hydrocracking. Industrial & Engineering Chemistry Research, 2019, 58, 7973-7979.	3.7	13
27	Dynamic one-dimensional pseudohomogeneous model for Fischer-Tropsch fixed-bed reactors. Fuel, 2019, 252, 371-392.	6.4	5
28	Defining appropriate reaction scheme for hydrotreating of vegetable oil through proper calculation of kinetic parameters. Fuel, 2019, 242, 167-173.	6.4	11
29	Comparison of mixing rules based on binary interaction parameters for calculating viscosity of crude oil blends. Fuel, 2019, 249, 198-205.	6.4	24
30	Modeling, simulation, and parametric sensitivity analysis of a commercial slurry-phase reactor for heavy oil hydrocracking. Fuel, 2019, 244, 258-268.	6.4	23
31	Sensitivity analysis of kinetic parameters for heavy oil hydrocracking. Fuel, 2019, 241, 836-844.	6.4	33
32	Comparison of hydrocracking kinetic models based on SARA fractions obtained in slurry-phase reactor. Fuel, 2019, 241, 495-505.	6.4	31
33	Viscosity Reduction of Heavy Oil during Slurryâ€Phase Hydrocracking. Chemical Engineering and Technology, 2019, 42, 148-155.	1.5	16
34	Effect of Reactor Configuration on the Hydrotreating of Atmospheric Residue. Energy & Energy	5.1	10
35	Effect of silicon incorporation method in the supports of NiMo catalysts for hydrotreating reactions. Fuel, 2019, 239, 1293-1303.	6.4	16
36	Experimental Study and Economic Analysis of Heavy Oil Partial Upgrading by Solvent Deasphalting–Hydrotreating. Energy & Fuels, 2018, 32, 55-59.	5.1	20

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37	Different alumina precursors in the preparation of supports for HDT and HDC of Maya crude oil. Catalysis Today, 2018, 305, 2-12.	4.4	12
38	Pyrolysis Kinetics of Heavy Oil Asphaltenes under Steam Atmosphere at Different Pressures. Energy & En	5.1	32
39	Modeling of CSTR and SPR small-scale isothermal reactors for heavy oil hydrocracking and hydrotreating. Fuel, 2018, 216, 852-860.	6.4	30
40	Modeling of hydrotreating catalyst deactivation for heavy oil hydrocarbons. Fuel, 2018, 225, 118-133.	6.4	62
41	Organic polymers as solid hydrogen donors in the hydrogenation of cyclohexene. Catalysis Today, 2018, 305, 143-151.	4.4	7
42	Batch Reactor Study of the Effect of Aromatic Diluents to Reduce Sediment Formation during Hydrotreating of Heavy Oil. Energy & E	5.1	14
43	Kinetic and Reactor Modeling of Catalytic Hydrotreatment of Vegetable Oils. Energy &	5.1	19
44	Dynamic Modeling and Simulation of a Slurry-Phase Reactor for Hydrotreating of Oil Fractions. Energy &	5.1	16
45	Modeling of Catalytic Fixed-Bed Reactors for Fuels Production by Fischer–Tropsch Synthesis. Energy & Lamp; Fuels, 2017, 31, 13011-13042.	5.1	15
46	Methods To Calculate Hydrogen Consumption during Hydrocracking Experiments in Batch Reactors. Energy &	5.1	15
47	Thermogravimetric Determination and Pyrolysis Thermodynamic Parameters of Heavy Oils and Asphaltenes. Energy & Discrete, 2017, 31, 10566-10575.	5.1	22
48	Characterization of Upgraded Oil Fractions Obtained by Slurry-Phase Hydrocracking at Low-Severity Conditions Using Analytical and Ore Catalysts. Energy & Energy & 2017, 31, 9162-9178.	5.1	11
49	Methods for determining asphaltene stability in crude oils. Fuel, 2017, 188, 530-543.	6.4	130
50	Experimental Methods for Developing Kinetic Models for Hydrocracking Reactions with Slurry-Phase Catalyst Using Batch Reactors. Energy & Samp; Fuels, 2016, 30, 4419-4437.	5.1	43
51	Use of Hydrogen Donors for Partial Upgrading of Heavy Petroleum. Energy & Samp; Fuels, 2016, 30, 9050-9060.	5.1	61
52	Required Viscosity Values To Ensure Proper Transportation of Crude Oil by Pipeline. Energy & Samp; Fuels, 2016, 30, 8850-8854.	5.1	63
53	Experimental Setups for Studying the Compatibility of Crude Oil Blends under Dynamic Conditions. Energy & Energ	5.1	16
54	Partial Upgrading of Heavy Crude Oil by Slurry-Phase Hydrocracking with Analytical Grade and Ore Catalysts. Energy & Ene	5.1	20

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55	Modeling of Slurry-Phase Reactors for Hydrocracking of Heavy Oils. Energy &	5.1	45
56	Dynamic modeling and simulation of a bench-scale reactor for the hydrocracking of heavy oil by using the continuous kinetic lumping approach. Reaction Kinetics, Mechanisms and Catalysis, 2016, 118, 299-311.	1.7	7
57	Calculating the Viscosity of Crude Oil Blends by Binary Interaction Parameters Using Literature Data. Petroleum Science and Technology, 2015, 33, 893-900.	1.5	13
58	Exploratory Study for the Upgrading of Transport Properties of Heavy Oil by Slurry-Phase Hydrocracking. Energy & Energy	5.1	23
59	Dynamic modeling and simulation of a naphtha catalytic reforming reactor. Applied Mathematical Modelling, 2015, 39, 764-775.	4.2	25
60	A review of experimental procedures for heavy oil hydrocracking with dispersed catalyst. Catalysis Today, 2014, 220-222, 274-294.	4.4	165
61	Current situation of emerging technologies for upgrading of heavy oils. Catalysis Today, 2014, 220-222, 248-273.	4.4	169
62	Modeling the kinetics of parallel thermal and catalytic hydrotreating of heavy oil. Fuel, 2014, 138, 27-36.	6.4	34
63	Hydrocracking of Maya crude oil in a slurry-phase batch reactor. II. Effect of catalyst load. Fuel, 2014, 130, 263-272.	6.4	53
64	Carbon and metal deposition during the hydroprocessing of Maya crude oil. Catalysis Today, 2014, 220-222, 97-105.	4.4	57
65	Maya crude oil hydrotreating reaction in a batch reactor using alumina-supported NiMo carbide and nitride as catalysts. Catalysis Today, 2014, 220-222, 318-326.	4.4	21
66	Modeling the deactivation by metal deposition of heavy oil hydrotreating catalyst. Catalysis Today, 2014, 220-222, 221-227.	4.4	13
67	Effect of alumina and silica–alumina supported NiMo catalysts on the properties of asphaltenes during hydroprocessing of heavy petroleum. Fuel, 2014, 138, 111-117.	6.4	15
68	Application of a three-stage approach for modeling the complete period of catalyst deactivation during hydrotreating of heavy oil. Fuel, 2014, 138, 45-51.	6.4	18
69	Kinetics of thermal hydrocracking of heavy oils under moderate hydroprocessing reaction conditions. Fuel, 2013, 110, 83-88.	6.4	27
70	Hydrodesulfurization activity of used hydrotreating catalysts. Fuel Processing Technology, 2013, 106, 453-459.	7.2	21
71	Transient behavior of residual oil front-end hydrodemetallization in a trickle-bed reactor. Chemical Engineering Journal, 2012, 197, 204-214.	12.7	16
72	Simulation and planning of a petroleum refinery based on carbon rejection processes. Fuel, 2012, 100, 80-90.	6.4	10

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73	Comparison of kinetic and reactor models to simulate a trickle-bed bench-scale reactor for hydrodesulfurization of VGO. Fuel, 2012, 100, 91-99.	6.4	19
74	Combined process schemes for upgrading of heavy petroleum. Fuel, 2012, 100, 110-127.	6.4	125
75	Modeling the performance of a bench-scale reactor sustaining HDS and HDM of heavy crude oil at moderate conditions. Fuel, 2012, 100, 152-162.	6.4	16
76	Kinetic model for hydrocracking of heavy oil in a CSTR involving short term catalyst deactivation. Fuel, 2012, 100, 193-199.	6.4	59
77	Modeling the Simultaneous Hydrodesulfurization and Hydrocracking of Heavy Residue Oil by using the Continuous Kinetic Lumping Approach. Energy & Energy & 2012, 26, 1999-2004.	5.1	16
78	Dynamic modeling and simulation of hydrotreating of gas oil obtained from heavy crude oil. Applied Catalysis A: General, 2012, 425-426, 13-27.	4.3	53
79	Genesis of Acidâ`Base Support Properties with Variations of Preparation Conditions: Cumene Cracking and Its Kinetics. Industrial & Engineering Chemistry Research, 2011, 50, 2715-2725.	3.7	20
80	Pyrolysis kinetics of atmospheric residue and its SARA fractions. Fuel, 2011, 90, 3602-3607.	6.4	108
81	Comparison of approaches to determine hydrogen consumption during catalytic hydrotreating of oil fractions. Fuel, 2011, 90, 3593-3601.	6.4	50
82	Testing various mixing rules for calculation of viscosity of petroleum blends. Fuel, 2011, 90, 3561-3570.	6.4	126
83	On the detailed solution and application of the continuous kinetic lumping modeling to hydrocracking of heavy oils. Fuel, 2011, 90, 3542-3550.	6.4	22
84	Modeling the effect of pressure and temperature on the hydrocracking of heavy crude oil by the continuous kinetic lumping approach. Applied Catalysis A: General, 2010, 382, 205-212.	4.3	29
85	Thermogravimetric determination of coke from asphaltenes, resins and sediments and coking kinetics of heavy crude asphaltenes. Catalysis Today, 2010, 150, 272-278.	4.4	104
86	A batch reactor study of the effect of deasphalting on hydrotreating of heavy oil. Catalysis Today, 2010, 150, 264-271.	4.4	21
87	A Review of Process Aspects and Modeling of Ebullated Bed Reactors for Hydrocracking of Heavy Oils. Catalysis Reviews - Science and Engineering, 2010, 52, 60-105.	12.9	54
88	NiMo supported acidic catalysts for heavy oil hydroprocessing. Catalysis Today, 2009, 141, 168-175.	4.4	49
89	Review on criteria to ensure ideal behaviors in trickle-bed reactors. Applied Catalysis A: General, 2009, 355, 1-19.	4.3	132
90	Application of continuous kinetic lumping modeling to moderate hydrocracking of heavy oil. Applied Catalysis A: General, 2009, 365, 237-242.	4.3	50

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91	Steadyâ€State and Dynamic Reactor Models for Hydrotreatment of Oil Fractions: A Review. Catalysis Reviews - Science and Engineering, 2009, 51, 485-607.	12.9	58
92	Vaporâ^'Liquid Equilibrium Study in Trickle-Bed Reactors. Industrial & Description Chemistry Research, 2009, 48, 1096-1106.	3.7	30
93	Evaluation of the hydrodynamics of high-pressure ebullated beds based on dimensional similitude. Catalysis Today, 2008, 130, 519-526.	4.4	9
94	Study of accelerated deactivation of hydrotreating catalysts by vanadium impregnation method. Catalysis Today, 2008, 130, 405-410.	4.4	14
95	Heavy crude oil hydroprocessing: A zeolite-based CoMo catalyst and its spent catalyst characterization. Catalysis Today, 2008, 130, 411-420.	4.4	43
96	Simulation and analysis of different quenching alternatives for an industrial vacuum gasoil hydrotreater. Chemical Engineering Science, 2008, 63, 662-673.	3.8	26
97	Comparison between refinery processes for heavy oil upgrading: a future fuel demand. International Journal of Oil, Gas and Coal Technology, 2008, 1, 250.	0.2	23
98	Comparison of Different Power-law Kinetic Models for Hydrocracking of Asphaltenes. Petroleum Science and Technology, 2007, 25, 263-275.	1.5	9
99	Easy Approach to Calculate Real Conversion and Yields from Hydroprocessing of Heavy Oils Plants. Energy & Energ	5.1	2
100	Hydrotreating of Maya Crude Oil: I. Effect of Support Composition and Its Pore-diameter on Asphaltene Conversion. Petroleum Science and Technology, 2007, 25, 187-199.	1.5	25
101	Hydrotreating of Maya Crude Oil: II. Generalized Relationship between Hydrogenolysis and HDAs. Petroleum Science and Technology, 2007, 25, 201-213.	1.5	14
102	Hydrodesulfurization, Hydrodenitrogenation, Hydrodemetallization, and Hydrodeasphaltenization of Maya Crude over NiMo/Al2O3 Modified with Ti and P. Petroleum Science and Technology, 2007, 25, 215-229.	1.5	17
103	Characterization of Asphaltenes from Hydrotreated Products by SEC, LDMS, MALDI, NMR, and XRD. Energy & SEC, LDMS, Energy & SEC, LDMS, MALDI, NMR, and XRD.	5.1	124
104	Comparison of Probability Distribution Functions for Fitting Distillation Curves of Petroleum. Energy & Samp; Fuels, 2007, 21, 2955-2963.	5.1	58
105	Sensitivity analysis based methodology to estimate the best set of parameters for heterogeneous kinetic models. Chemical Engineering Journal, 2007, 128, 85-93.	12.7	64
106	Mathematical modeling and simulation of hydrotreating reactors: Cocurrent versus countercurrent operations. Applied Catalysis A: General, 2007, 332, 8-21.	4.3	57
107	Heavy oil hydroprocessing over supported NiMo sulfided catalyst: An inhibition effect by added H2S. Fuel, 2007, 86, 1263-1269.	6.4	39
108	A review of recent advances on process technologies for upgrading of heavy oils and residua. Fuel, 2007, 86, 1216-1231.	6.4	794

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109	Reactors for Hydroprocessing. Chemical Industries, 2007, , 71-120.	0.1	20
110	Dynamic Modeling and Simulation of Catalytic Hydrotreating Reactors. Energy & Energy	5.1	65
111	Characteristics of Maya crude hydrodemetallization and hydrodesulfurization catalysts. Catalysis Today, 2005, 104, 86-93.	4.4	62
112	Kinetics of asphaltenes conversion during hydrotreating of Maya crude. Catalysis Today, 2005, 109, 99-103.	4.4	52
113	A comparative study for heavy oil hydroprocessing catalysts at micro-flow and bench-scale reactors. Catalysis Today, 2005, 109, 24-32.	4.4	40
114	Experimental and theoretical determination of the particle size of hydrotreating catalysts of different shapes. Catalysis Today, 2005, 109, 120-127.	4.4	19
115	Kinetic modeling of hydrocracking of heavy oil fractions: A review. Catalysis Today, 2005, 109, 76-92.	4.4	195
116	Pressure and temperature effects on the hydrodynamic characteristics of ebullated-bed systems. Catalysis Today, 2005, 109, 205-213.	4.4	27
117	Hydroprocessing of heavy petroleum feeds: Tutorial. Catalysis Today, 2005, 109, 3-15.	4.4	197
118	Process heat integration of a heavy crude hydrotreatment plant. Catalysis Today, 2005, 109, 214-218.	4.4	22
119	A batch reactor study to determine effectiveness factors of commercial HDS catalyst. Catalysis Today, 2005, 104, 70-75.	4.4	42
120	Effect of hydrotreating conditions on Maya asphaltenes composition and structural parameters. Catalysis Today, 2005, 109, 178-184.	4.4	47
121	Kinetic Model for Moderate Hydrocracking of Heavy Oils. Industrial & Engineering Chemistry Research, 2005, 44, 9409-9413.	3.7	144
122	Simulation of an isothermal hydrodesulfurization small reactor with different catalyst particle shapes. Catalysis Today, 2004, 98, 243-252.	4.4	69
123	Cumene cracking functionalities on sulfided Co(Ni)Mo/TiO2-SiO2 catalysts. Applied Catalysis A: General, 2004, 258, 215-225.	4.3	30
124	On the effect of reaction conditions on liquid phase sulfiding of a NiMo HDS catalyst. Catalysis Today, 2004, 98, 75-81.	4.4	37
125	Effect of alumina preparation on hydrodemetallization and hydrodesulfurization of Maya crude. Catalysis Today, 2004, 98, 151-160.	4.4	70
126	Hydrotreating of diluted Maya crude with NiMo/Al2O3-TiO2 catalysts: effect of diluent composition. Catalysis Today, 2004, 98, 171-179.	4.4	36

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127	Modeling of Hydrodesulfurization (HDS), Hydrodenitrogenation (HDN), and the Hydrogenation of Aromatics (HDA) in a Vacuum Gas Oil Hydrotreater. Energy & Ener	5.1	92
128	Alumina–titania binary mixed oxide used as support of catalysts for hydrotreating of Maya heavy crude. Applied Catalysis A: General, 2003, 244, 141-153.	4.3	60
129	Alumina-silica binary mixed oxide used as support of catalysts for hydrotreating of Maya heavy crude. Applied Catalysis A: General, 2003, 250, 231-238.	4.3	34
130	Catalysts for hydroprocessing of Maya heavy crude. Applied Catalysis A: General, 2003, 253, 125-134.	4.3	31
131	Changes in Asphaltene Properties during Hydrotreating of Heavy Crudes. Energy & Changes in Asphaltene Properties during Hydrotreating of Heavy Crudes. Energy & Changes in Asphaltene Properties during Hydrotreating of Heavy Crudes. Energy & Changes in Asphaltene Properties during Hydrotreating of Heavy Crudes. Energy & Changes in Asphaltene Properties during Hydrotreating of Heavy Crudes. Energy & Changes in Asphaltene Properties during Hydrotreating of Heavy Crudes. Energy & Changes in Asphaltene Properties during Hydrotreating of Heavy Crudes. Energy & Changes in Asphaltene Properties during Hydrotreating of Heavy Crudes. Energy & Changes in Asphaltene Properties during Hydrotreating of Heavy Crudes.	5.1	141
132	Catalyst Deactivation during Hydroprocessing of Maya Heavy Crude Oil. 1. Evaluation at Constant Operating Conditions. Energy & En	5.1	69
133	Changes in Apparent Reaction Order and Activation Energy in the Hydrodesulfurization of Real Feedstocks. Energy & Energy	5.1	59
134	Simulation of a Commercial Semiregenerative Reforming Plant Using Feedstocks with and without Benzene Precursors. Chemical Engineering and Technology, 2002, 25, 541-546.	1.5	17
135	On the Use of Steady-State Optimal Initial Operating Conditions for Control Scheme Implementation of a Fixed-Bed Fischer–Tropsch Reactor. Arabian Journal for Science and Engineering, 0, , 1.	3.0	0