

# Jorge Ancheyta

## List of Publications by Year in descending order

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135  
papers

6,116  
citations

71102

41  
h-index

85541

71  
g-index

141  
all docs

141  
docs citations

141  
times ranked

2771  
citing authors

#	ARTICLE	IF	CITATIONS
1	A review of recent advances on process technologies for upgrading of heavy oils and residua. Fuel, 2007, 86, 1216-1231.	6.4	794
2	Hydroprocessing of heavy petroleum feeds: Tutorial. Catalysis Today, 2005, 109, 3-15.	4.4	197
3	Kinetic modeling of hydrocracking of heavy oil fractions: A review. Catalysis Today, 2005, 109, 76-92.	4.4	195
4	Current situation of emerging technologies for upgrading of heavy oils. Catalysis Today, 2014, 220-222, 248-273.	4.4	169
5	A review of experimental procedures for heavy oil hydrocracking with dispersed catalyst. Catalysis Today, 2014, 220-222, 274-294.	4.4	165
6	Kinetic Model for Moderate Hydrocracking of Heavy Oils. Industrial & Engineering Chemistry Research, 2005, 44, 9409-9413.	3.7	144
7	Changes in Asphaltene Properties during Hydrotreating of Heavy Crudes. Energy & Fuels, 2003, 17, 1233-1238.	5.1	141
8	Review on criteria to ensure ideal behaviors in trickle-bed reactors. Applied Catalysis A: General, 2009, 355, 1-19.	4.3	132
9	Methods for determining asphaltene stability in crude oils. Fuel, 2017, 188, 530-543.	6.4	130
10	Testing various mixing rules for calculation of viscosity of petroleum blends. Fuel, 2011, 90, 3561-3570.	6.4	126
11	Combined process schemes for upgrading of heavy petroleum. Fuel, 2012, 100, 110-127.	6.4	125
12	Characterization of Asphaltenes from Hydrotreated Products by SEC, LDMS, MALDI, NMR, and XRD. Energy & Fuels, 2007, 21, 2121-2128.	5.1	124
13	Pyrolysis kinetics of atmospheric residue and its SARA fractions. Fuel, 2011, 90, 3602-3607.	6.4	108
14	Thermogravimetric determination of coke from asphaltenes, resins and sediments and coking kinetics of heavy crude asphaltenes. Catalysis Today, 2010, 150, 272-278.	4.4	104
15	Modeling of Hydrodesulfurization (HDS), Hydrodenitrogenation (HDN), and the Hydrogenation of Aromatics (HDA) in a Vacuum Gas Oil Hydrotreater. Energy & Fuels, 2004, 18, 789-794.	5.1	92
16	Effect of alumina preparation on hydrodemetallization and hydrodesulfurization of Maya crude. Catalysis Today, 2004, 98, 151-160.	4.4	70
17	Catalyst Deactivation during Hydroprocessing of Maya Heavy Crude Oil. 1. Evaluation at Constant Operating Conditions. Energy & Fuels, 2002, 16, 1438-1443.	5.1	69
18	Simulation of an isothermal hydrodesulfurization small reactor with different catalyst particle shapes. Catalysis Today, 2004, 98, 243-252.	4.4	69

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19	Dynamic Modeling and Simulation of Catalytic Hydrotreating Reactors. Energy & Fuels, 2006, 20, 936-945.	5.1	65
20	Sensitivity analysis based methodology to estimate the best set of parameters for heterogeneous kinetic models. Chemical Engineering Journal, 2007, 128, 85-93.	12.7	64
21	Required Viscosity Values To Ensure Proper Transportation of Crude Oil by Pipeline. Energy & Fuels, 2016, 30, 8850-8854.	5.1	63
22	Characteristics of Maya crude hydrodemetallization and hydrodesulfurization catalysts. Catalysis Today, 2005, 104, 86-93.	4.4	62
23	Modeling of hydrotreating catalyst deactivation for heavy oil hydrocarbons. Fuel, 2018, 225, 118-133.	6.4	62
24	Use of Hydrogen Donors for Partial Upgrading of Heavy Petroleum. Energy & Fuels, 2016, 30, 9050-9060.	5.1	61
25	Alumina-titania binary mixed oxide used as support of catalysts for hydrotreating of Maya heavy crude. Applied Catalysis A: General, 2003, 244, 141-153.	4.3	60
26	Changes in Apparent Reaction Order and Activation Energy in the Hydrodesulfurization of Real Feedstocks. Energy & Fuels, 2002, 16, 189-193.	5.1	59
27	Kinetic model for hydrocracking of heavy oil in a CSTR involving short term catalyst deactivation. Fuel, 2012, 100, 193-199.	6.4	59
28	Comparison of Probability Distribution Functions for Fitting Distillation Curves of Petroleum. Energy & Fuels, 2007, 21, 2955-2963.	5.1	58
29	Steady-State and Dynamic Reactor Models for Hydrotreatment of Oil Fractions: A Review. Catalysis Reviews - Science and Engineering, 2009, 51, 485-607.	12.9	58
30	Mathematical modeling and simulation of hydrotreating reactors: Cocurrent versus countercurrent operations. Applied Catalysis A: General, 2007, 332, 8-21.	4.3	57
31	Carbon and metal deposition during the hydroprocessing of Maya crude oil. Catalysis Today, 2014, 220-222, 97-105.	4.4	57
32	A Review of Process Aspects and Modeling of Ebullated Bed Reactors for Hydrocracking of Heavy Oils. Catalysis Reviews - Science and Engineering, 2010, 52, 60-105.	12.9	54
33	Dynamic modeling and simulation of hydrotreating of gas oil obtained from heavy crude oil. Applied Catalysis A: General, 2012, 425-426, 13-27.	4.3	53
34	Hydrocracking of Maya crude oil in a slurry-phase batch reactor. II. Effect of catalyst load. Fuel, 2014, 130, 263-272.	6.4	53
35	Kinetics of asphaltenes conversion during hydrotreating of Maya crude. Catalysis Today, 2005, 109, 99-103.	4.4	52
36	Application of continuous kinetic lumping modeling to moderate hydrocracking of heavy oil. Applied Catalysis A: General, 2009, 365, 237-242.	4.3	50

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37	Comparison of approaches to determine hydrogen consumption during catalytic hydrotreating of oil fractions. <i>Fuel</i> , 2011, 90, 3593-3601.	6.4	50
38	NiMo supported acidic catalysts for heavy oil hydroprocessing. <i>Catalysis Today</i> , 2009, 141, 168-175.	4.4	49
39	Effect of hydrotreating conditions on Maya asphaltenes composition and structural parameters. <i>Catalysis Today</i> , 2005, 109, 178-184.	4.4	47
40	Modeling of Slurry-Phase Reactors for Hydrocracking of Heavy Oils. <i>Energy &amp; Fuels</i> , 2016, 30, 2525-2543.	5.1	45
41	Heavy crude oil hydroprocessing: A zeolite-based CoMo catalyst and its spent catalyst characterization. <i>Catalysis Today</i> , 2008, 130, 411-420.	4.4	43
42	Experimental Methods for Developing Kinetic Models for Hydrocracking Reactions with Slurry-Phase Catalyst Using Batch Reactors. <i>Energy &amp; Fuels</i> , 2016, 30, 4419-4437.	5.1	43
43	A batch reactor study to determine effectiveness factors of commercial HDS catalyst. <i>Catalysis Today</i> , 2005, 104, 70-75.	4.4	42
44	A comparative study for heavy oil hydroprocessing catalysts at micro-flow and bench-scale reactors. <i>Catalysis Today</i> , 2005, 109, 24-32.	4.4	40
45	Heavy oil hydroprocessing over supported NiMo sulfided catalyst: An inhibition effect by added H <sub>2</sub> S. <i>Fuel</i> , 2007, 86, 1263-1269.	6.4	39
46	On the effect of reaction conditions on liquid phase sulfiding of a NiMo HDS catalyst. <i>Catalysis Today</i> , 2004, 98, 75-81.	4.4	37
47	Hydrotreating of diluted Maya crude with NiMo/Al <sub>2</sub> O <sub>3</sub> -TiO <sub>2</sub> catalysts: effect of diluent composition. <i>Catalysis Today</i> , 2004, 98, 171-179.	4.4	36
48	Alumina-silica binary mixed oxide used as support of catalysts for hydrotreating of Maya heavy crude. <i>Applied Catalysis A: General</i> , 2003, 250, 231-238.	4.3	34
49	Modeling the kinetics of parallel thermal and catalytic hydrotreating of heavy oil. <i>Fuel</i> , 2014, 138, 27-36.	6.4	34
50	Sensitivity analysis of kinetic parameters for heavy oil hydrocracking. <i>Fuel</i> , 2019, 241, 836-844.	6.4	33
51	Pyrolysis Kinetics of Heavy Oil Asphaltenes under Steam Atmosphere at Different Pressures. <i>Energy &amp; Fuels</i> , 2018, 32, 1132-1138.	5.1	32
52	Kinetic models for Fischer-Tropsch synthesis for the production of clean fuels. <i>Catalysis Today</i> , 2020, 353, 3-16.	4.4	32
53	Catalysts for hydroprocessing of Maya heavy crude. <i>Applied Catalysis A: General</i> , 2003, 253, 125-134.	4.3	31
54	Comparison of hydrocracking kinetic models based on SARA fractions obtained in slurry-phase reactor. <i>Fuel</i> , 2019, 241, 495-505.	6.4	31

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55	Cumene cracking functionalities on sulfided Co(Ni)Mo/TiO <sub>2</sub> -SiO <sub>2</sub> catalysts. <i>Applied Catalysis A: General</i> , 2004, 258, 215-225.	4.3	30
56	Vapor-Liquid Equilibrium Study in Trickle-Bed Reactors. <i>Industrial &amp; Engineering Chemistry Research</i> , 2009, 48, 1096-1106.	3.7	30
57	Modeling of CSTR and SPR small-scale isothermal reactors for heavy oil hydrocracking and hydrotreating. <i>Fuel</i> , 2018, 216, 852-860.	6.4	30
58	Kinetic modeling of aquathermolysis for upgrading of heavy oils. <i>Fuel</i> , 2022, 310, 122286.	6.4	30
59	Modeling the effect of pressure and temperature on the hydrocracking of heavy crude oil by the continuous kinetic lumping approach. <i>Applied Catalysis A: General</i> , 2010, 382, 205-212.	4.3	29
60	Pressure and temperature effects on the hydrodynamic characteristics of ebullated-bed systems. <i>Catalysis Today</i> , 2005, 109, 205-213.	4.4	27
61	Kinetics of thermal hydrocracking of heavy oils under moderate hydroprocessing reaction conditions. <i>Fuel</i> , 2013, 110, 83-88.	6.4	27
62	Simulation and analysis of different quenching alternatives for an industrial vacuum gasoil hydrotreater. <i>Chemical Engineering Science</i> , 2008, 63, 662-673.	3.8	26
63	Hydrotreating of Maya Crude Oil: I. Effect of Support Composition and Its Pore-diameter on Asphaltene Conversion. <i>Petroleum Science and Technology</i> , 2007, 25, 187-199.	1.5	25
64	Dynamic modeling and simulation of a naphtha catalytic reforming reactor. <i>Applied Mathematical Modelling</i> , 2015, 39, 764-775.	4.2	25
65	Comparison of mixing rules based on binary interaction parameters for calculating viscosity of crude oil blends. <i>Fuel</i> , 2019, 249, 198-205.	6.4	24
66	Comparison between refinery processes for heavy oil upgrading: a future fuel demand. <i>International Journal of Oil, Gas and Coal Technology</i> , 2008, 1, 250.	0.2	23
67	Exploratory Study for the Upgrading of Transport Properties of Heavy Oil by Slurry-Phase Hydrocracking. <i>Energy &amp; Fuels</i> , 2015, 29, 9-15.	5.1	23
68	Modeling, simulation, and parametric sensitivity analysis of a commercial slurry-phase reactor for heavy oil hydrocracking. <i>Fuel</i> , 2019, 244, 258-268.	6.4	23
69	Process heat integration of a heavy crude hydrotreatment plant. <i>Catalysis Today</i> , 2005, 109, 214-218.	4.4	22
70	On the detailed solution and application of the continuous kinetic lumping modeling to hydrocracking of heavy oils. <i>Fuel</i> , 2011, 90, 3542-3550.	6.4	22
71	Thermogravimetric Determination and Pyrolysis Thermodynamic Parameters of Heavy Oils and Asphaltenes. <i>Energy &amp; Fuels</i> , 2017, 31, 10566-10575.	5.1	22
72	A batch reactor study of the effect of deasphalting on hydrotreating of heavy oil. <i>Catalysis Today</i> , 2010, 150, 264-271.	4.4	21

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73	Hydrodesulfurization activity of used hydrotreating catalysts. <i>Fuel Processing Technology</i> , 2013, 106, 453-459.	7.2	21
74	Maya crude oil hydrotreating reaction in a batch reactor using alumina-supported NiMo carbide and nitride as catalysts. <i>Catalysis Today</i> , 2014, 220-222, 318-326.	4.4	21
75	SARA-based kinetic model for non-catalytic aquathermolysis of heavy crude oil. <i>Journal of Petroleum Science and Engineering</i> , 2022, 216, 110845.	4.2	21
76	Genesis of Acid-Base Support Properties with Variations of Preparation Conditions: Cumene Cracking and Its Kinetics. <i>Industrial &amp; Engineering Chemistry Research</i> , 2011, 50, 2715-2725.	3.7	20
77	Partial Upgrading of Heavy Crude Oil by Slurry-Phase Hydrocracking with Analytical Grade and Ore Catalysts. <i>Energy &amp; Fuels</i> , 2016, 30, 10117-10125.	5.1	20
78	Experimental Study and Economic Analysis of Heavy Oil Partial Upgrading by Solvent Deasphalting-Hydrotreating. <i>Energy &amp; Fuels</i> , 2018, 32, 55-59.	5.1	20
79	Reactors for Hydroprocessing. <i>Chemical Industries</i> , 2007, , 71-120.	0.1	20
80	Experimental and theoretical determination of the particle size of hydrotreating catalysts of different shapes. <i>Catalysis Today</i> , 2005, 109, 120-127.	4.4	19
81	Comparison of kinetic and reactor models to simulate a trickle-bed bench-scale reactor for hydrodesulfurization of VGO. <i>Fuel</i> , 2012, 100, 91-99.	6.4	19
82	Kinetic and Reactor Modeling of Catalytic Hydrotreatment of Vegetable Oils. <i>Energy &amp; Fuels</i> , 2018, 32, 7245-7261.	5.1	19
83	Application of a three-stage approach for modeling the complete period of catalyst deactivation during hydrotreating of heavy oil. <i>Fuel</i> , 2014, 138, 45-51.	6.4	18
84	Simulation of a Commercial Semiregenerative Reforming Plant Using Feedstocks with and without Benzene Precursors. <i>Chemical Engineering and Technology</i> , 2002, 25, 541-546.	1.5	17
85	Hydrodesulfurization, Hydrodenitrogenation, Hydrodemetallization, and Hydrodeasphaltenization of Maya Crude over NiMo/Al <sub>2</sub> O <sub>3</sub> Modified with Ti and P. <i>Petroleum Science and Technology</i> , 2007, 25, 215-229.	1.5	17
86	Transient behavior of residual oil front-end hydrodemetallization in a trickle-bed reactor. <i>Chemical Engineering Journal</i> , 2012, 197, 204-214.	12.7	16
87	Modeling the performance of a bench-scale reactor sustaining HDS and HDM of heavy crude oil at moderate conditions. <i>Fuel</i> , 2012, 100, 152-162.	6.4	16
88	Modeling the Simultaneous Hydrodesulfurization and Hydrocracking of Heavy Residue Oil by using the Continuous Kinetic Lumping Approach. <i>Energy &amp; Fuels</i> , 2012, 26, 1999-2004.	5.1	16
89	Experimental Setups for Studying the Compatibility of Crude Oil Blends under Dynamic Conditions. <i>Energy &amp; Fuels</i> , 2016, 30, 8216-8225.	5.1	16
90	Dynamic Modeling and Simulation of a Slurry-Phase Reactor for Hydrotreating of Oil Fractions. <i>Energy &amp; Fuels</i> , 2017, 31, 5691-5700.	5.1	16

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91	Viscosity Reduction of Heavy Oil during Slurry-Phase Hydrocracking. <i>Chemical Engineering and Technology</i> , 2019, 42, 148-155.	1.5	16
92	Effect of silicon incorporation method in the supports of NiMo catalysts for hydrotreating reactions. <i>Fuel</i> , 2019, 239, 1293-1303.	6.4	16
93	Effect of alumina and silica- alumina supported NiMo catalysts on the properties of asphaltenes during hydroprocessing of heavy petroleum. <i>Fuel</i> , 2014, 138, 111-117.	6.4	15
94	Modeling of Catalytic Fixed-Bed Reactors for Fuels Production by Fischer-Tropsch Synthesis. <i>Energy &amp; Fuels</i> , 2017, 31, 13011-13042.	5.1	15
95	Methods To Calculate Hydrogen Consumption during Hydrocracking Experiments in Batch Reactors. <i>Energy &amp; Fuels</i> , 2017, 31, 11690-11697.	5.1	15
96	Revisiting the importance of appropriate parameter estimation based on sensitivity analysis for developing kinetic models. <i>Fuel</i> , 2020, 267, 117113.	6.4	15
97	Evaluation of mixing rules to predict viscosity of petrodiesel and biodiesel blends. <i>Fuel</i> , 2021, 283, 118941.	6.4	15
98	Evaluation of Asphaltene Stability of a Wide Range of Mexican Crude Oils. <i>Energy &amp; Fuels</i> , 2021, 35, 408-418.	5.1	15
99	Hydrotreating of Maya Crude Oil: II. Generalized Relationship between Hydrogenolysis and HDAs. <i>Petroleum Science and Technology</i> , 2007, 25, 201-213.	1.5	14
100	Study of accelerated deactivation of hydrotreating catalysts by vanadium impregnation method. <i>Catalysis Today</i> , 2008, 130, 405-410.	4.4	14
101	Batch Reactor Study of the Effect of Aromatic Diluents to Reduce Sediment Formation during Hydrotreating of Heavy Oil. <i>Energy &amp; Fuels</i> , 2018, 32, 60-66.	5.1	14
102	Modeling the deactivation by metal deposition of heavy oil hydrotreating catalyst. <i>Catalysis Today</i> , 2014, 220-222, 221-227.	4.4	13
103	Calculating the Viscosity of Crude Oil Blends by Binary Interaction Parameters Using Literature Data. <i>Petroleum Science and Technology</i> , 2015, 33, 893-900.	1.5	13
104	Using Separate Kinetic Models to Predict Liquid, Gas, and Coke Yields in Heavy Oil Hydrocracking. <i>Industrial &amp; Engineering Chemistry Research</i> , 2019, 58, 7973-7979.	3.7	13
105	Modeling and control of a Fischer-Tropsch synthesis fixed-bed reactor with a novel mechanistic kinetic approach. <i>Chemical Engineering Journal</i> , 2020, 390, 124489.	12.7	13
106	Different alumina precursors in the preparation of supports for HDT and HDC of Maya crude oil. <i>Catalysis Today</i> , 2018, 305, 2-12.	4.4	12
107	Evaluation and comparison of thermodynamic and kinetic parameters for oxidation and pyrolysis of Yarega heavy crude oil asphaltenes. <i>Fuel</i> , 2021, 297, 120703.	6.4	12
108	Characterization of Upgraded Oil Fractions Obtained by Slurry-Phase Hydrocracking at Low-Severity Conditions Using Analytical and Ore Catalysts. <i>Energy &amp; Fuels</i> , 2017, 31, 9162-9178.	5.1	11

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109	Defining appropriate reaction scheme for hydrotreating of vegetable oil through proper calculation of kinetic parameters. <i>Fuel</i> , 2019, 242, 167-173.	6.4	11
110	Regular solution model to predict the asphaltenes flocculation and sediments formation during hydrocracking of heavy oil. <i>Fuel</i> , 2020, 260, 116160.	6.4	11
111	Simulation and planning of a petroleum refinery based on carbon rejection processes. <i>Fuel</i> , 2012, 100, 80-90.	6.4	10
112	Effect of Reactor Configuration on the Hydrotreating of Atmospheric Residue. <i>Energy &amp; Fuels</i> , 2019, 33, 1649-1658.	5.1	10
113	Modeling of a bench-scale fixed-bed reactor for catalytic hydrotreating of vegetable oil. <i>Renewable Energy</i> , 2020, 148, 790-797.	8.9	10
114	Hydrodeoxygenation of vegetable oil in batch reactor: Experimental considerations. <i>Chinese Journal of Chemical Engineering</i> , 2020, 28, 1670-1683.	3.5	10
115	Kinetics of heavy oil non-catalytic aquathermolysis with and without stoichiometric coefficients. <i>Fuel</i> , 2022, 323, 124365.	6.4	10
116	Analysis of kinetic models for hydrocracking of heavy oils for In-situ and Ex-situ applications. <i>Fuel</i> , 2022, 323, 124322.	6.4	10
117	Comparison of Different Power-law Kinetic Models for Hydrocracking of Asphaltenes. <i>Petroleum Science and Technology</i> , 2007, 25, 263-275.	1.5	9
118	Evaluation of the hydrodynamics of high-pressure ebullated beds based on dimensional similitude. <i>Catalysis Today</i> , 2008, 130, 519-526.	4.4	9
119	Catalyst Stacking Technology as a Viable Solution to Ultralow Sulfur Diesel Production. <i>Energy &amp; Fuels</i> , 2022, 36, 3201-3218.	5.1	8
120	Dynamic modeling and simulation of a bench-scale reactor for the hydrocracking of heavy oil by using the continuous kinetic lumping approach. <i>Reaction Kinetics, Mechanisms and Catalysis</i> , 2016, 118, 299-311.	1.7	7
121	Organic polymers as solid hydrogen donors in the hydrogenation of cyclohexene. <i>Catalysis Today</i> , 2018, 305, 143-151.	4.4	7
122	Catalytic hydrocracking of a Mexican heavy oil on a MoS <sub>2</sub> /Al <sub>2</sub> O <sub>3</sub> catalyst: I. Study of the transformation of isolated saturates fraction obtained from SARA analysis. <i>Catalysis Today</i> , 2020, 353, 153-162.	4.4	6
123	Thermogravimetric Determination of the Kinetics of Petroleum Needle Coke Formation by Decantoil Thermolysis. <i>ACS Omega</i> , 2020, 5, 29570-29576.	3.5	6
124	Dynamic one-dimensional pseudohomogeneous model for Fischer-Tropsch fixed-bed reactors. <i>Fuel</i> , 2019, 252, 371-392.	6.4	5
125	State estimation for heavy oil hydroprocessing reactors using extended Kalman filters. <i>Fuel</i> , 2020, 262, 116565.	6.4	5
126	Scaling Up the Performance of a Reactor Model for Hydrotreating Vegetable Oil from Bench-Scale to Pilot-Scale Reactors. <i>Industrial &amp; Engineering Chemistry Research</i> , 2020, 59, 21712-21719.	3.7	5



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127	Prediction of Temperature Profiles for Catalytic Hydrotreating of Vegetable Oil with a Robust Dynamic Reactor Model. <i>Industrial &amp; Engineering Chemistry Research</i> , 2021, 60, 13812-13821.	3.7	4
128	Selection of heavy oil upgrading technologies by proper estimation of petroleum prices. <i>Petroleum Science and Technology</i> , 2022, 40, 217-236.	1.5	4
129	Modeling and simulation of a multi-bed industrial reactor for renewable diesel hydroprocessing. <i>Renewable Energy</i> , 2022, 186, 173-182.	8.9	4
130	Batch Reactor Study for Partial Upgrading of a Heavy Oil with a Novel Solid Hydrogen Transfer Agent. <i>Energy &amp; Fuels</i> , 2020, 34, 15714-15726.	5.1	3
131	Simulation of bench-scale hydrotreating of vegetable oil reactor under non-isothermal conditions. <i>Fuel</i> , 2020, 275, 117960.	6.4	3
132	Easy Approach to Calculate Real Conversion and Yields from Hydroprocessing of Heavy Oils Plants. <i>Energy &amp; Fuels</i> , 2007, 21, 1824-1825.	5.1	2
133	Importance of proper hydrodynamics modelling in fixed-bed reactors: Fischer-Tropsch synthesis study case. <i>Canadian Journal of Chemical Engineering</i> , 2019, 97, 2685-2698.	1.7	2
134	Modeling of the Deasphalting Process by a Residue-Solvent Equilibrium Calculation Using Continuous Thermodynamics. <i>Industrial &amp; Engineering Chemistry Research</i> , 2022, 61, 3383-3394.	3.7	1
135	On the Use of Steady-State Optimal Initial Operating Conditions for Control Scheme Implementation of a Fixed-Bed Fischer-Tropsch Reactor. <i>Arabian Journal for Science and Engineering</i> , 0, , 1.	3.0	0